Removal of Azo Dye from Aqueous Solutions using Chitosan

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ABSTRACT

Adsorption of Congo Red (CR) from aqueous solution onto chitosan was investigated in a batch system. The effects of solution pH, initial dye concentration, and temperature were studied. Results indicated that chitosan could be used as a biosorbent to remove the azo dyes from contaminated water. Synthesis of chitosan involved three main stages as preconditioning, demineralization, deproteinization and deacetylation. Chitosan was characterized using Fourier Transform Infrared Spectroscopy (FTIR) and solubility in 1% acetic acid.

Key words: Adsorption; Congo red; Chitosan, synthesized.

INTRODUCTION

The chemical contamination of water from a wide range of toxic derivatives is an important environmental problem. Synthetic dyes usually have a complex aromatic molecular structure, which possibly comes from coal-tar based hydrocarbons such as benzene, naphthalene, toluene, xylene, etc. The complex aromatic molecular structures of dyes make them more stable and more difficult to biodegrade. It is known that wastewaters containing dyes are very difficult to treat, since the dyes are recalcitrant molecules (particularly azo dyes), resistant to aerobic digestion, and are stable to oxidizing agents. Textile, paper, plastics, and cosmetic industries use a wide variety of dyes to color their products and discharge large amount of effluents including dyes which are very toxic and could cause serious ecological problems. Therefore, dye pollution in water stream is a major environmental problem.

The methods of dye removal from industrial wastewaters could require many processes such as biological treatment, coagulation, electrochemical techniques, adsorption, and oxidation. Among these methods, adsorption is considered an effective and economical method to remove dyes from wastewaters. It has been reported that many different types of adsorbents are effective in removing color from aqueous effluents. Natural
polymeric materials are gaining more and more interest for application as adsorbents in wastewater treatment due to their biodegradable and non-toxic nature. Currently, the most common procedure involves the use of activated carbon\textsuperscript{12}. Activated carbon is regarded as an effective but expensive adsorbent due to the high cost of manufacturing and regeneration. Because of its relatively high cost, there have been attempts to utilize low cost and naturally occurring adsorbents. There are many different studies on the use of low cost materials such as various agricultural wastes\textsuperscript{13-15}, Chitosan (CS) offers an interesting set of characteristics, including non-toxicity, biodegradability, biocompatibility, and bioactivity.

Chitosan and its derivatives have been extensively investigated as biosorbents (figure 1) for removal of heavy metals and dyes\textsuperscript{16-20}.

The overall objective of this study is to investigate the dye removal from wastewater by adsorption using chitosan. The specific objectives included; synthesize chitosan from fish shells and removal of Congo red dye using as a bio-adsorption material.

**MATERIALS AND METHODS**

**Preparation of Sorbent**

Traditional isolation of chitin consists of four traditional steps (Figure 2): demineralization (DM), deproteinization (DP), decolorization (DC), and deacetylation (DA).

**Preparation of Adsorbent**

Congo red contains an azo (-N=N-) chromophore and an acidic auxochrome (sulfonate : -SO3H) (which, respectively, gives and reinforces the coloration) associated with the benzene structure. Congo red is a the sodium salt of a derivative of benzidine and naphthionic acid as in figure 3.

**Batch adsorption experiments**

A stock solution of CR (1.0 g/L) was prepared by dissolving 1 g of CR powder in 1 L of double distilled water. The desired concentrations ranging from 10 to 60 mg/L were obtained by dilution. For each adsorption experiment, 50 ml of the dye solution with a specified concentration was stirred at 100 rpm in a glass flask. The pH of solutions was adjusted to a desired value by adding 0.1 mol/L NaOH or HCl solution. Batch adsorption experiments were carried out using a thermostated shaker for a certain contact time at a determined temperature at 100 rpm. At predetermined time intervals, samples were withdrawn by a pipette and centrifuged at 4000 rpm. Then, the residual concentration was determined from a constructed calibration curve by measuring the absorbance at $\lambda_{\text{max}} = 498$ nm using UV-Vis spectrophotometer.

Batch adsorption experiments were carried out to examine effects of adsorbent dosage, initial dye concentration, solution pH, and time on the adsorption of CR on chitosan.

The amount of CR adsorbed on chitosan (at a predetermined time $t$), $q_t$ (in mg/g), was determined using the mass balance equation:

$$q_t = (C_0 - C_t) \times \frac{m}{V}$$  \hspace{1cm} (1)

The decolorization rate ($\mu$) of CR was calculated by the following equation:

$$\mu = \frac{C_0 - C_t}{C_0} \times 100\%$$  \hspace{1cm} (2)

where $C_0$ is the initial concentration of CR (in mg/L), $C_t$ (in mg/L) is the instant concentration of CR at a predetermined time $t$, $V$ is the volume of the solution (in L), and $m$ is the mass chitosan (in g).

**RESULTS AND DISCUSSION**

**Effect of adsorbent dosage**

The effect of adsorbent dosage (varied from 0.025 to 0.25 gm) on the percentage removal of 50 mg/L CR solution is shown in Fig. 3. The percentage removal of CR from the solution increased from 30% to 86% as the adsorbent dosage increased from 0.025 to 0.25 gm. This result is expected because of the increased adsorbent surface area and availability of more adsorption sites caused by increasing adsorbent dosage\textsuperscript{23,24}.

**Effect of solution pH**

The pH of the dye solution affects the surface charge of the adsorbent, the degree of
Fig. 1: Chemical structures of chitin, chitosan and cellulose

Fig. 2: Traditional Chitosan Production

- Wet crawfish shell
- Washing and drying
- Grinding and sieving
- Deproteinization
  - 3% NaOH (w/v)
  - for 1h at b.p., solid:
    - solvent (1:10, w/v)
- Washing
- Demineralization
  - 1N HCl for 30 min at room temp., solid:
    - solvent (1:15, w/v)
- Washing and Drying
- Deacetylation
  - 5% NaOH for 2hr at 90°C
  - solid:solvent (1:10, w/v)
- Washing and Drying
- Chitosan

The percentage removal of CR at different pH values is plotted in Fig. 4. The percentage removal increased from 24.29% to 80.85% when pH was decreased from 10 to 2. This was because the CR molecule (with one sulfuric group) ionized easily even in acidic media and became a soluble CR anion. As the initial solution pH decreased, the number of positively charged active sites increased due to the protonation of the amine groups (–NH₂) in the CS chain. Consequently, the electrostatic interaction between the positively charged adsorbent and the CR anions increased, which resulted in increased adsorption. Furthermore, the lower adsorption removal percentage at alkaline pH contributed to the presence of excess hydroxyl ions, which competed with the CR molecules for adsorption sites. In contrast, as expressed in equilibrium equation (3), the quinoid structure of CR is more easily reduced than its azo structure. Therefore, higher removal percentages were observed at acidic pH values for CR adsorption.

Effect of contact time

A 50ml of 50mg/L of CR dye was taken in conical flasks and treated with 0.1 gm chitosan (adsorbent) at several times (20, 40, 60, 80, 100, 120 and 140 min.), the variation in percent removal of dye with the time was shown in figure 5. The ionization of the materials, and the dissociation of functional groups on the active sites of the adsorbent. As well, it affects the structure of the dye molecule. The percentage removal of CR at different pH values is plotted in Fig. 4. The percentage removal increased from 24.29% to 80.85% when pH was decreased from 10 to 2. This was because the CR molecule (with one sulfuric group) ionized easily even in acidic media and became a soluble CR anion. As the initial solution pH decreased, the number of positively charged active sites increased due to the protonation of the amine groups (–NH₂) in the CS chain. Consequently, the electrostatic interaction between the positively charged adsorbent and the CR anions increased, which resulted in increased adsorption. Furthermore, the lower adsorption removal percentage at alkaline pH contributed to the presence of excess hydroxyl ions, which competed with the CR molecules for adsorption sites. In contrast, as expressed in equilibrium equation (3), the quinoid structure of CR is more easily reduced than its azo structure. Therefore, higher removal percentages were observed at acidic pH values for CR adsorption.
percentage removal increased from 31.41% to 80.60% when time was increased from 20 to 140 min., this due to saturation of active sites which do not allow further adsorption to take place\textsuperscript{27}.

Effect of initial CR concentration

The effect of initial CR concentration on the percentage removal of the dye is shown in figure 6. The initial CR concentration was varied from 10 to 60 mg/L. A rapid initial adsorption of CR took place within the first 20 min, after which the adsorption slowed down and then almost reached equilibrium at 120 min. The percentage of CR removal evidently decreased with increasing initial dye concentration. The percentage removal was 82.05% for 10 mg/L initial concentration, and only 30.26% for 60 mg/L after 120 min of adsorption (figure 6). This was caused by an increase in the mass gradient.
CONCLUSIONS

The synthesis of chitosan involved three main stages: demineralization, deproteinization, and deacetylation. It was characterized by using Fourier Transform Infrared Spectroscopy (FTIR) and solubility in 1% acetic acid. CR adsorption onto the chitosan depended highly on adsorbent dosage, initial dye concentration, solution pH and time.

REFERENCES